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# The Effect of Air Preheat at Atmospheric Pressure on the Formation of No<sub>x</sub> in the Quick-Mix Sections of an Axially Staged Combustor

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### **Summary**

The Rich-burn/Quick—mix/Lean-burn (RQL) combustor concept has been proposed to minimize the formation of nitrogen oxides ( $NO_x$ ) in gas turbine systems. The success of this combustor strategy is dependent upon the efficiency of the mixing section bridging the fuel-rich and fuel-lean stages. Note that although these results were obtained from an experiment designed to study an RQL mixer, the link between mixing and  $NO_x$  signatures is considerably broader than this application, in that the need to understand this link exists in most advanced combustors. The experiment reported herein was designed to study the effects of inlet air temperature on  $NO_x$  formation in a mixing section. The results indicate that  $NO_x$  emission is increased for all preheated cases compared to non-preheated cases. When comparing the various mixing modules, the affect of jet penetration is important, as this determines where  $NO_x$  concentrations peak, and affects overall  $NO_x$  production. Although jet air comprises 70 percent of the total airflow, the impact that jet air preheat has on overall  $NO_x$  emissions is small compared to preheating both main and jet air flow.

### **Nomenclature**

DR jet-to-mainstream density ratio

d orifice axial height, or round hole diameter

f<sub>avg</sub> average planar jet mixture fraction derived from carbon mass fraction

f<sub>var</sub> planar jet mixture fraction variance

J jet-to-mainstream momentum-flux ratio =  $(\rho V^2)_{iets}/(\rho U^2)_{main}$ 

MR jet-to-mainstream mass-flow ratio

n number of round holes in quick-mix module

R radius of the quick-mix module

r radial distance from the module center

T<sub>iet</sub> average jet air temperature

T<sub>main</sub> average mainstream temperature

U mainstream velocity

U<sub>S</sub> spatial unmixedness

V jet velocity

V<sub>ref</sub> reference velocity

x axial distance from leading edge of orifice

Y mass fraction of carbon

φ equivalence ratio = (fuel/air)<sub>local</sub>/(fuel/air)<sub>stoichiometric</sub>

### Introduction

Many processes involved in the injection of fuel and in the control of exhaust temperature rely on jet mixing with a crossflow of gas to mix fluid streams. One particular application in which jet mixing in a confined crossflow plays a fundamental role is the Rich-burn/Quick-mix/Lean-burn (RQL) combustor. The success of this combustor in producing lower emissions than conventional gas turbine combustors depends on the efficiency of the mixing section bridging the fuel-rich and fuel-lean stages of combustion. In this combustor design, the jets of air introduced into the quick-mix section should mix with the fuel-rich reacting crossflow as quickly as possible to bring the reaction to an overall fuel-lean equivalence ratio. It is hypothesized that rapid and spatially distributed mixing must occur in order to prevent the formation of hot pockets (consisting either of closer to stoichiometric species concentrations, higher temperatures, or both) which in turn drive pollutant formation.

Previous studies (refs. 1 and 2) involved the construction of a facility, and reported results for reacting tests in cylindrical crossflow configurations at atmospheric pressure. The current study expands upon this initial work by elevating the inlet air temperatures, testing various mixing module designs and studying the species concentrations, with particular interest in  $NO_x$  formation.

### **Background**

Numerous studies on the jet in crossflow problem have yielded insight on such flow field characteristics as the jet structure and penetration, the development of vortices, the jet entrainment of crossflow fluid, and the flow field distributions resulting from jet mixing. An extensive listing of documented jet-in-crossflow studies performed in the past few decades can be found in references 3 to 6. Note that many of the studies cited in these summaries are of a single jet in an unbounded crossflow or are otherwise inappropriate for direct application. Although the single jet is a key component in combustor flow fields, these flows are usually confined, and interaction between jets is critical. Also, because the references listed in references 3 to 6 are extensive, only those papers from which specific material is mentioned will be cited in this paper.

In previous studies (refs. 5 and 6), nonreacting experiments and modeling were often used as convenient tools to explore the mixing of air jets into the fuel-rich cross stream. The primary goal of these studies was to determine orifice configurations that lead to optimal mixing within a specified duct length. In a cylindrical duct geometry, experimental surveys of the effect of the jet-to-crossflow momentum-flux ratio and the shape, orientation, and number of orifices on mixing were performed in order to gain a mechanistic understanding of jet penetration and mixing dynamics (ref. 7). A systematic optimization scheme using a design of experiments statistical approach was applied to the experimental data to determine the round hole configurations

leading to optimal mixing at various momentum-flux ratios. For jet-to-mainstream momentum-flux ratios of 36 and 70, the number of round holes leading to optimal mixing were identified as 10 and 15, respectively (ref. 8).

While extensive nonreacting confined jet mixing work has been performed (see refs. 3 to 6), research into reacting flows has been limited. Tests on multiple jet mixing in reacting flows have been performed on model gas turbine combustors of a can-type, or cylindrical duct geometry. In many of these experiments (refs. 9 to 13), the model gas turbine combustors contained two sets of holes for primary and dilution air mixing typical of conventional combustors, as opposed to the single stage quick mixing scheme. These studies were also concerned with varying operating conditions such as fuel injection (ref. 9), air preheat (ref. 10), fuel-air ratio (ref. 11), or the momentum-flux ratio of the primary jets (ref. 12). In one study, a geometric parameterization was pursued, but was related to varying the positions of the rows of the primary and dilution jets rather than with changing the orifice configurations (ref. 12). An experiment performed on a model RQL combustor operating at various pressures and inlet temperatures did yield  $NO_x$  emissions measurements for a 20 round hole mixing section (ref. 13). The results from this RQL study also emphasized that the optimization of the quick-mixing section was integral to lowering the total  $NO_x$  emissions from the RQL combustor. On the whole, these reacting tests varied operating parameters in order to affect the distributions of emissions and temperature.

Archival journal publications of NO formation in the RQL concept have been few (refs. 13 and 14), however, the results of these studies have shown that momentum flux ratio and orifice configuration as being the leading factors in  $NO_x$  formation.

Initial reacting flow experiments studied by the authors included the flowfield of a row of jets mixing with rich reacting gases confined to a cylindrical crossflow (refs. 1 and 2). The work presented here expands upon the reacting flow investigation by using the diagnostic and analysis techniques developed in the previous study. The objective for this study is to examine orifice configurations that demonstrated optimal mixing in previous tests, and vary the inlet temperatures to measure the impact this change has on species concentrations.

### **Experiment**

### **Facility**

The experimental facility used consisted of a premixing zone, a fuel-rich combustion zone, and a jet-mixing section as shown in figure 1. In the premixing zone propane gas is mixed with air upstream of the ignition point. Fuel-rich combustion occurs downstream of the quarl in a zone stabilized by a swirl-induced recirculation zone. To dissipate the swirl in the flow and to introduce a uniform nonswirling flow into the jet-mixing section, the fuel-rich product was passed through an oxide-bonded silicon carbide (OBSiC) ceramic foam matrix (Hi-Tech Ceramics) with a rated porosity of 10 pores/in.

The jet mixing section was comprised of a modular quartz section to which jet air is supplied from a surrounding plenum. The plenum was fed by four equally-spaced, air ports located toward the base of the plenum. A high-temperature steel flow-straightener installed in the plenum conditioned and equally distributed, the jet air entering the mixing module.

To supply the necessary heated air, two recirculating heaters were utilized. The main-air line and jet-air line were heated by a 20 and 25 kW heater, respectively. Each heater is capable of

supplying the required maximum of 260 °C (500 °F) air preheat temperature at the desired flowrates.

The quartz modules which comprised the jet mixing section were 280 mm (11 in.) in length, with inner and outer wall diameters of 80 mm (3.15 in.) and 85 mm (3.35 in.). The row of orifices was positioned with its centerline 115 mm (4.5 in.) downstream from the module entrance. An alumina-silica blend of ceramic fiber paper provides sealing between the quartz module and the stainless steel mating surfaces to form the air plenum for the jets. Modules tested were 8, 12, 14, and 22-orifice configurations.

### Measurements

The purpose of the present investigation was to examine the impact of air preheat on species concentrations of O<sub>2</sub>, CO<sub>2</sub>, CO, HC and NO<sub>x</sub>. Species concentrations are obtained downstream of the jet air injection plane.

Species concentration data were obtained in a sector grid for the plane at x/R = 1 (plane 5 in refs. 1 and 2) for each module. The x/R = 1 plane is measured from the leading edge of the orifices.

Each planar grid consisted of 16 points spread over a region that includes two orifices (fig. 2(b)). The points include one point located at the center, and five points along each of the arc lengths at r/R = 1/3, 2/3, and 1. The points along each arc are distributed such that two points are aligned with the center of the orifices and three are aligned with the midpoint between orifice centers for all cases.

Species concentration measurements are obtained by sampling through a water-cooled stainless-steel probe by routing the sample through a heated line connected to the emission analyzers. Water was condensed from the gas before the sample is analyzed by chemiluminesence for NO (nondispersed infrared) NDIR analysis for CO, and CO<sub>2</sub>, paramagnetic analysis for O<sub>2</sub>, and flame ionization detection (FID) for total hydrocarbons.

### **Experimental Conditions**

The experiments were performed for a jet-to-mainstream momentum-flux ratio (J) of 57 and a mass-flow ratio (MR) of 2.5. The total effective area of the mixing module orifices is 9 cm<sup>2</sup>  $(1.4 \text{ in.}^2)$ . The ratio of the total effective jet area to cross-sectional area is 0.18. The rich equivalence ratio and overall equivalence ratio are 1.66 and 0.45, respectively. The operating pressure for the system is one atmosphere.

Various levels of preheat were applied to both the jet and main airflows. Inlet temperature operating conditions for the experiment are noted in table I. The results show comparisons between non-preheated air, preheated jet air only, and preheated jet and main air cases.

### **Analyses**

The jet mixture fraction was derived from conserved scalar calculations of the mass fraction of carbon. As a step toward obtaining the carbon mass fraction at each datum point, the wet mole fraction was calculated from the dry species concentration measurements. The wet mole fractions were obtained by solving a system of eight linear equations for the measured dry species

concentrations of CO, CO<sub>2</sub>, O<sub>2</sub>, and unburned HC (assumed to be comprised mainly of unburned  $C_3H_8$ ), as well as for  $C_2H_4$ ,  $H_2$ ,  $N_2$ , and  $H_2O$  (ref. 15). The inclusion of  $C_2H_4$ , which is a prevalent intermediate species produced from the combustion of  $C_3H_8$  (ref. 16) was necessary in order to form a closed set of equations. The calculated unburned hydrocarbon species  $C_3H_8$  and  $C_2H_4$  contributed, at most, to 1.4 percent of the overall wet mole fraction at each point. The concentration of  $H_2$ , a primary species of combustion produced under fuel-rich reactions, was assumed to be 65 percent of the concentration of CO (ref. 15).  $N_2$  was assumed to make up the rest of the gas concentration in the sample.

### **Results and Discussion**

The  $NO_x$  data are presented in the following sequence: (1) the effect of air preheat showing a comparison of  $NO_x$  emissions for each test condition, and (2) a comparison of the experimental configurations (i.e., the various mixing modules) for each preheat test condition. The former will show the general trends observed with all of the modules tested, and the latter will illustrate the contrast between the mixing modules for a given test condition.

### **Effect of Preheat**

The effect of heating the inlet air on the measured  $NO_x$  values is illustrated in figure 3. Non-preheated air data was collected as a baseline to determine the effect air preheat has on  $NO_x$ , and to repeat the (unpublished) experiments of MYL in 1997 to ensure experimental repeatability. Mainstream measurements s of CO and  $CO_2$ , 11 and 5 percent respectively, were virtually unaffected by preheat, and were consistent with equilibrium values.  $NO_x$  measurements were also consistent with equilibrium calculations and were 2 ppmv without preheat, and 13 ppmv for  $500\,^{\circ}$ F preheat. Due to the dilution through the mixing section, one would expect a  $NO_x$  concentration of only 4 ppmv at the exit for mainstream preheat if no  $NO_x$  were formed in the mixer.

Most notable of the comparison between the preheated jet air case, and the preheated main and jet air case of figure 3, is the small impact of preheated jet air on  $NO_x$ . The jet air comprises over 70 percent of the total airflow, but preheating jet air results in relatively small increases in  $NO_x$  emissions compared to the main and jet preheated air case.

Figure 4 presents the corresponding  $NO_x$  distribution plots. These plots also show the effect that jet penetration has on determining the locations for peak  $NO_x$  formation. Both the linear and contour plots indicate peak  $NO_x$  formations occurring near the orifices of the module (in the wakes of the jets).

The distributions of equivalence ratio are given in figure 5. Note that preheat has very little effect on jet penetration, and that the equivalence ratio distributions (refs. 12 and 13) better reflect the mixing than do to the NO<sub>x</sub> distributions, as the latter are similar for each module.

To account more accurately for the overall effect of preheated air on  $NO_x$  formation for a given case, area weighted averages were calculated. The overall effect of preheating only jet air, and both main and jet air preheat on the production of  $NO_x$  is shown in figure 6. This figure shows clearly that the affect of jet air preheat, with a  $NO_x$  value of 16 ppmv (for the 14 hole module), is relatively smaller than that of the main and jet air preheat case, with a  $NO_x$  value of 24 ppmv.

### **Round Hole Module Comparisons**

Overall Combustion Performance.—Figures 7 to 9 present the concentrations of O<sub>2</sub>, CO, CO<sub>2</sub> and hydrocarbons for the four modules that were tested (8, 12, 14, and 22 round hole modules) for no preheat (fig. 7), jet air preheat (fig. 8), and jet and main preheated air (fig. 9) conditions. The corresponding distribution plots are shown in figures 10 to 12. In each case, the trends are very similar and the differences that do exist are a result of jet penetration for that particular module (see also fig. 5). The penetration of the jets for the 12 and 14 hole module cases is observed to be different than that of the 22 hole module case as indicated by the flatness, or smoothness, of the data. Similar measurements were observed for the non-preheat air condition and the jet air preheat condition with relatively small differences in the major species concentrations as shown in figures 7 to 12.

Jet Air Preheat.—Previous studies indicated optimal mixing configurations for round hole modules (refs. 1 and 2). The current work compares the various modules for given experimental conditions (nonpreheat, jet air preheat, and main and jet air preheat) to determine which modules produce lower  $NO_x$  emissions. The data presented in figures 13(a) to (c) were obtained for the jet air preheat experimental condition and shows that the various modules have similar overall  $NO_x$  performance. Similar spatial distributions of  $NO_x$  are observed for each module with the exception of the center region where the 14 round hole module shows slightly higher  $NO_x$  emissions. This difference is illustrated in the area weighted average chart (fig. 13(c)) with the 14 round hole module producing slightly higher  $NO_x$  than the 12 and 22 round hole module cases. It should be noted that the differences are only 2 to 4 ppmv.

*Main & Jet Air Preheat*.—The results of the main and jet air preheat experimental conditions are similar to the jet air preheat results. The data for each module, figures 14(a) and (b), follow almost identical paths with the exception of the 22 round hole module. In this case, the  $NO_x$  seems to be a little less near the center region. This may be due to the fact that the 22 round hole module is considered a very overpenetrating mixing module, and thus may have lower  $NO_x$  formation in this region.

The overall effect of main and jet air preheat experimental conditions is presented in figure 14 showing a slightly different trend than the jet air preheat case. The data indicates that the 12 round hole module has highest  $NO_x$  concentrations compared to the 14 and 22 round hole modules. As with the jet air preheat cases the difference between the largest and smallest overall  $NO_x$  emissions is only 3.5 ppmv.

### **Summary and Conclusions**

An experiment was performed to expand upon earlier work by incorporating preheated inlet air, and examining the effect it has on  $NO_x$  production. The following was revealed in the experiment:

- Jet penetration determines where NO<sub>x</sub> concentrations peak and affects overall NO<sub>x</sub> production.
- Jet air comprises over 70 percent of the total airflow, however the impact of preheating jet air alone on overall NO<sub>x</sub> emissions is small compared to preheating both main and jet air. This is likely due increased sensitivity of NO<sub>x</sub> kinetics to increases in the fuel rich zone temperatures leading to increased production of fixed nitrogen species.

 Overall NO<sub>x</sub> concentration varies little with mixing configuration. However, there is a tradeoff with CO production especially for under-penetrating configurations such as the 22 round hole module.

These results show that preheating both main and jet air increases  $NO_x$  significantly more than preheating only the jet air. Also, the four mixing strategies investigated showed a small difference in overall  $NO_x$  concentration although these configurations ranged from those giving underto overpenetrating jets.

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TABLE I.—OPERATING CONDITIONS

Description	Inlet air temperature, °C	
	(°F)	
Nonpreheated air	22 (72)	
Jet air preheat	260 (500)	
Main and jet air preheat	260 (500)	

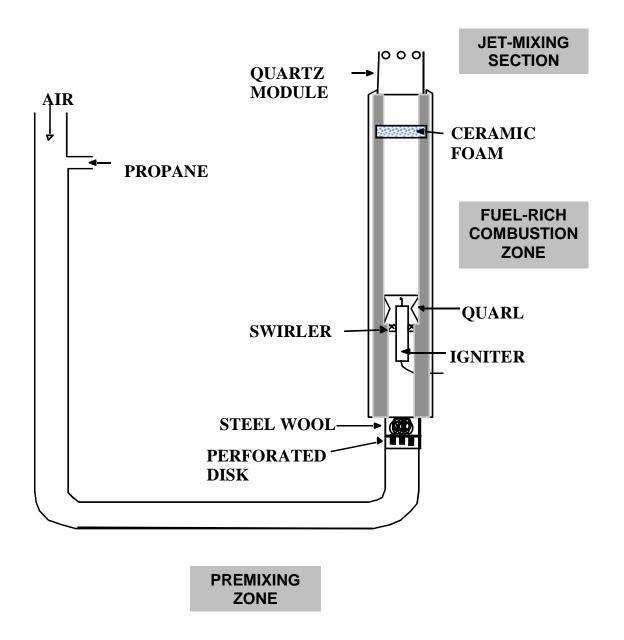
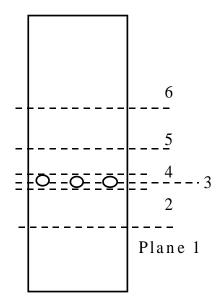
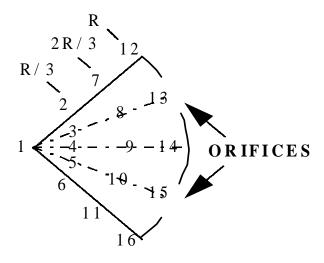


Figure 1. Schematic of Experimental Rich Product Generator with Quartz RQL module.



# (a) Data plane locations



## (b) Data point locations

**Figure 2. Measurement Locations** 

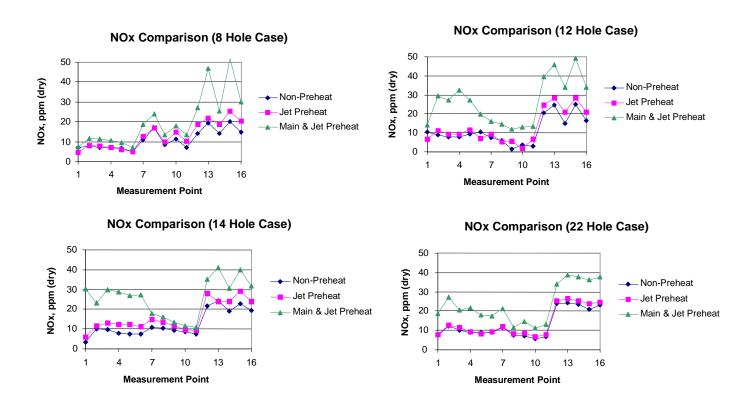
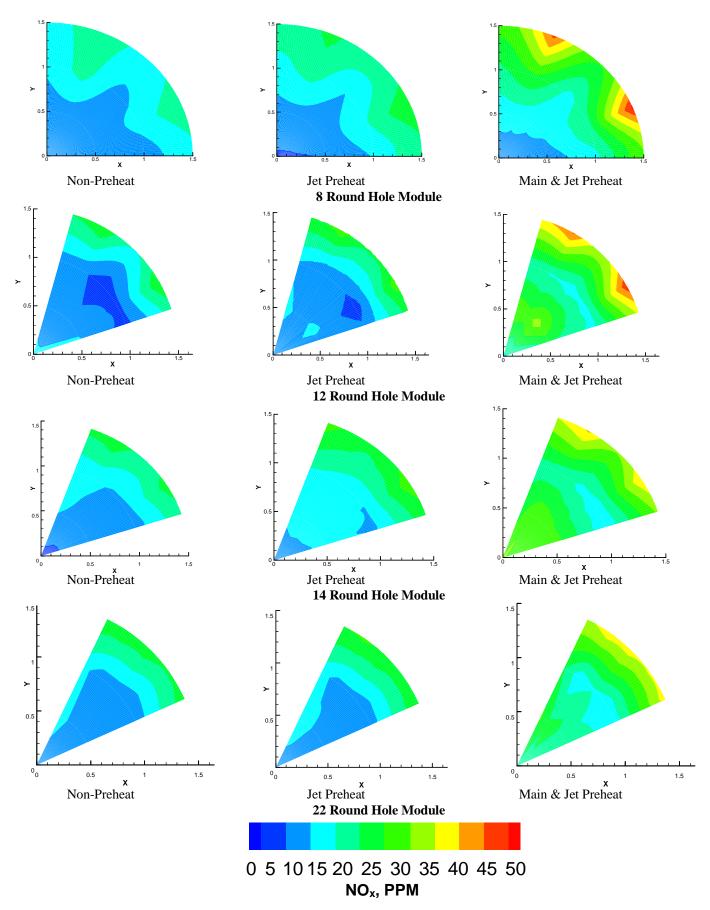


Figure 3.  $NO_X$  Measurement Plots



 $Figure~4.~NO_X~Distribution~Plots~for~Non-Preheated, Jet~Air~Preheat, and~Main~\&~Jet~Air~Preheat~Conditions\\for~the~four~modules~tested$ 

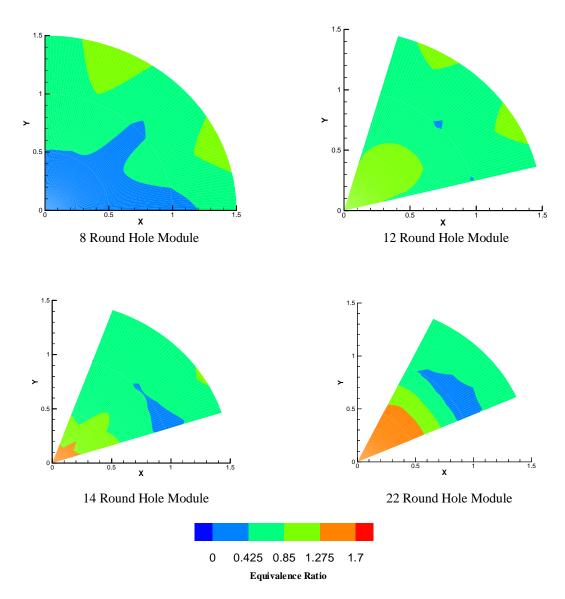


Figure 5. Non-Preheat Case Equivalence Ratio Distribution Plots

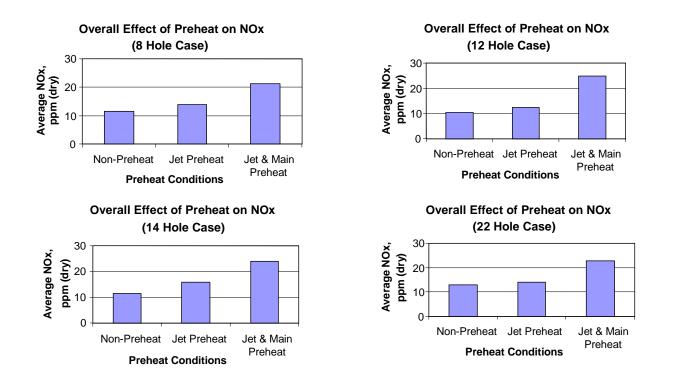


Figure 6. Area Weighted Planar Average NO<sub>X</sub> Data

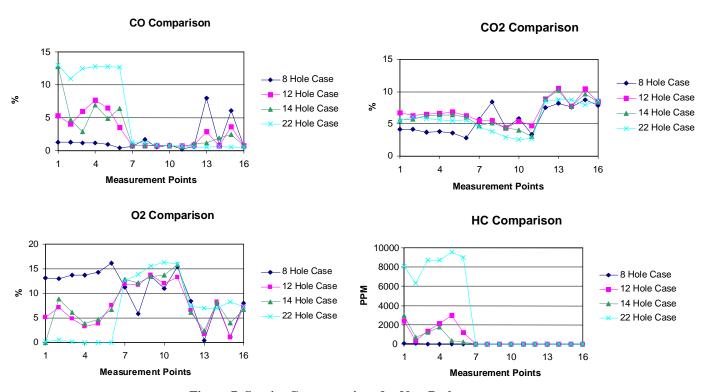


Figure 7. Species Concentrations for Non-Preheat

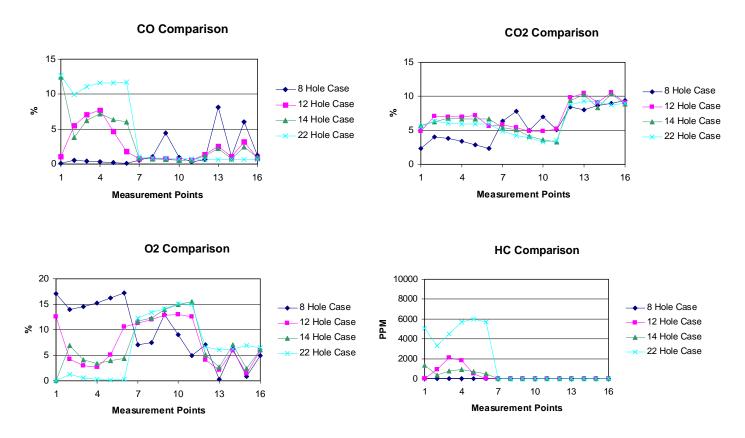


Figure 8. Species Concentration for Jet Air Preheat

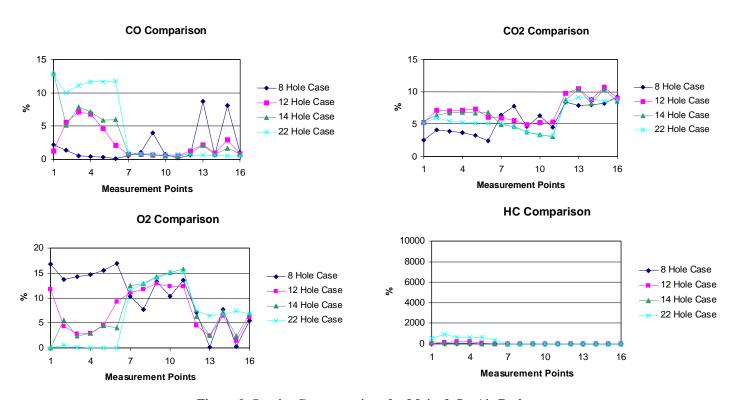
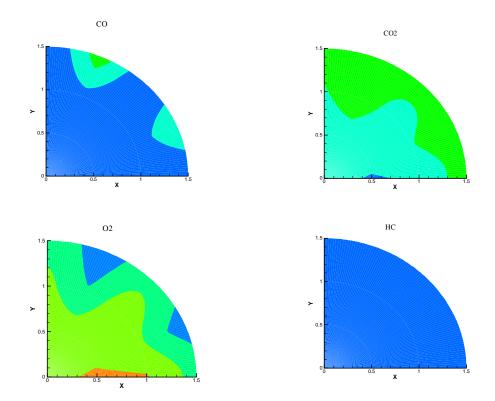
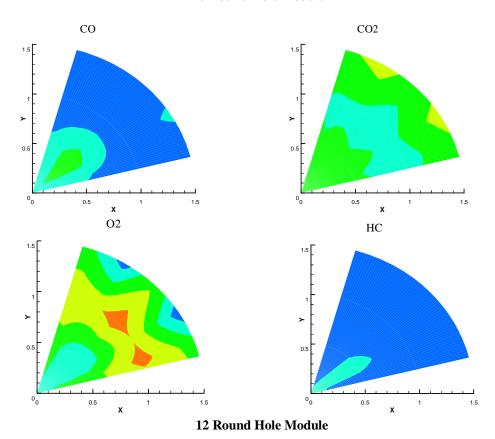
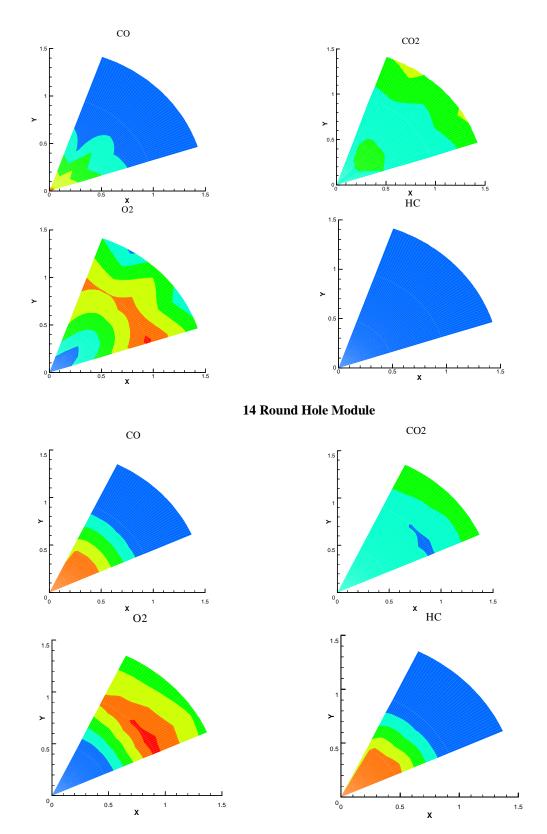


Figure 9. Species Concentrations for Main & Jet Air Preheat



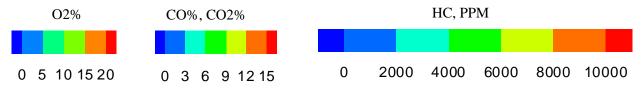
### **8 Round Hole Module**

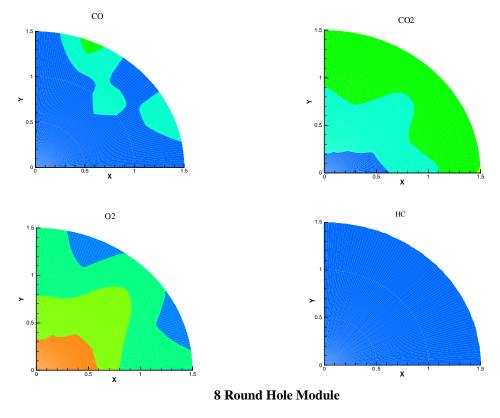


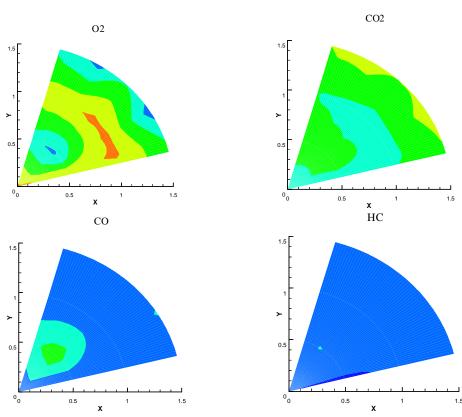


22 Round Hole Module

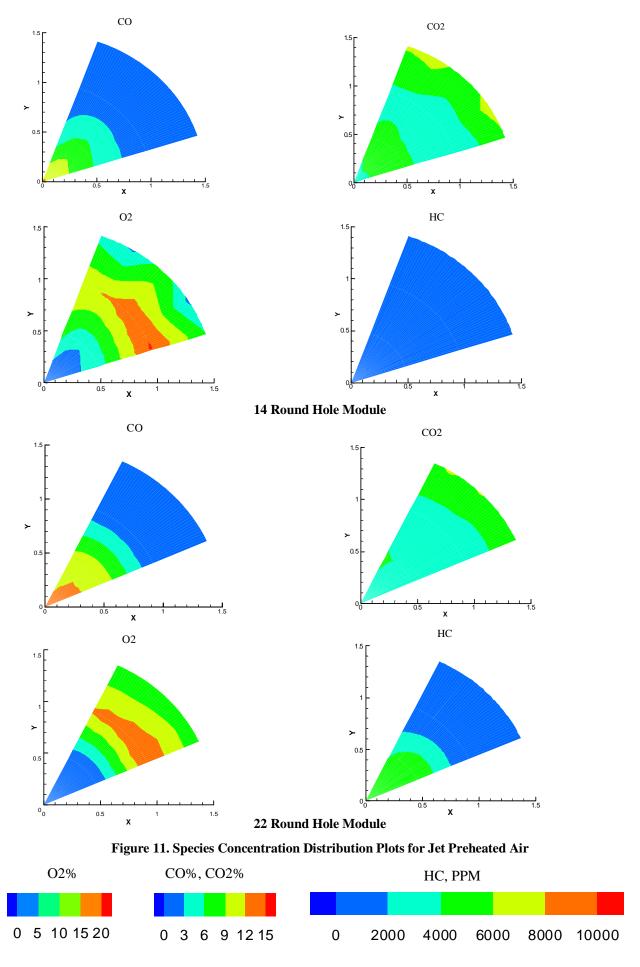
Figure 10. Species Concentration Distribution Plots for Non-Preheated Air

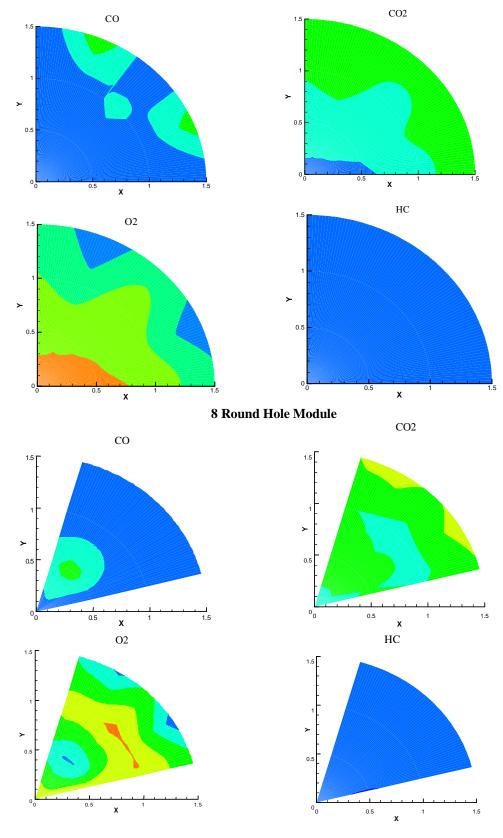




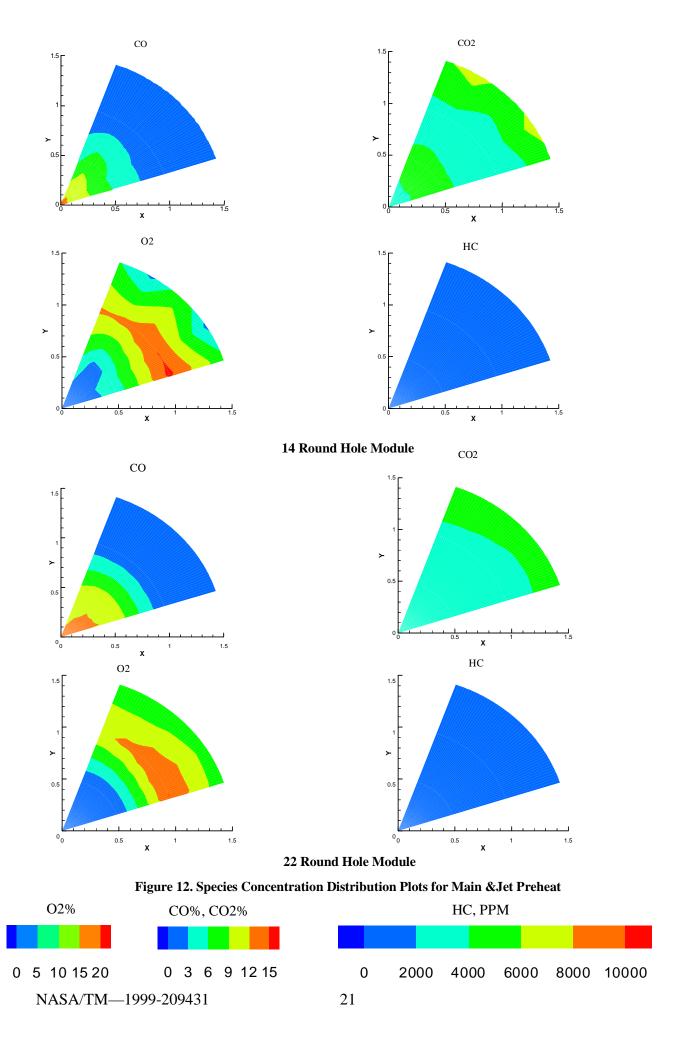


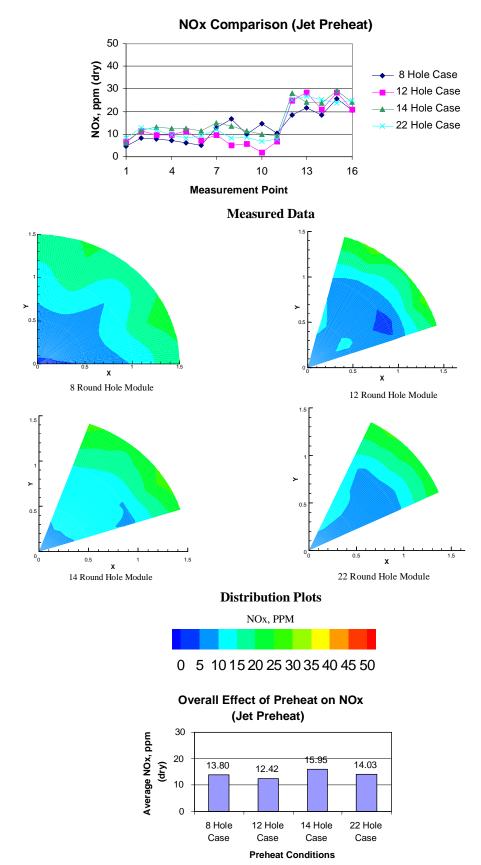
12 Round Hole Module



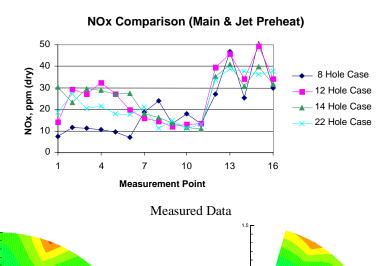


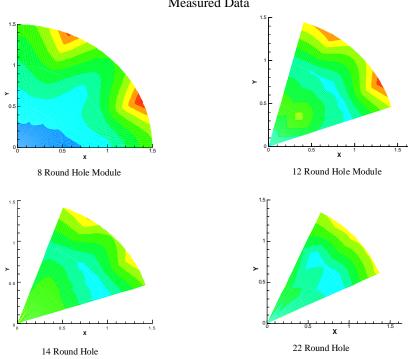
12 Round Hole Module

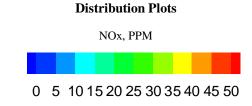


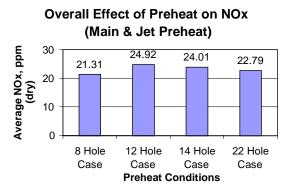


Area Weighted Planar Averages
Figure 13. NO<sub>X</sub> Comparison for Jet Air Preheat









Area weighted Planar Averages Figure 14 NO<sub>x</sub> Comparison for Main &Jet Air Preheat

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### 13. ABSTRACT (Maximum 200 words)

The Rich-burn/Quick—mix/Lean-burn (RQL) combustor concept has been proposed to minimize the formation of nitrogen oxides ( $NO_x$ ) in gas turbine systems. The success of this combustor strategy is dependent upon the efficiency of the mixing section bridging the fuel-rich and fuel-lean stages. Note that although these results were obtained from an experiment designed to study an RQL mixer, the link between mixing and  $NO_x$  signatures is considerably broader than this application, in that the need to understand this link exists in most advanced combustors. The experiment reported herein was designed to study the effects of inlet air temperature on  $NO_x$  formation in a mixing section. The results indicate that  $NO_x$  emission is increased for all preheated cases compared to non-preheated cases. When comparing the various mixing modules, the affect of jet penetration is important, as this determines where  $NO_x$  concentrations peak, and affects overall  $NO_x$  production. Although jet air comprises 70 percent of the total airflow, the impact that jet air preheat has on overall  $NO_x$  emissions is small compared to preheating both main and jet air flow.

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